WELCOME TO THE CALLIDUS COMBUSTION SCHOOL 2020

YOU ARE AT THE RIGHT PLACE, PLEASE WAIT A MOMENT AND THE PRESENTATION WILL BEGIN AT THE APPOINTED TIME

CallidusPartsInquiries@Honeywell.com



Time	Monday, October 5, 2020	Tuesday, October 6, 2020	Wednesday, October 7, 2020	Thursday, October 8, 2020
10:00 AM CDT	Process Burner and Heater Combustion Fundamentals	Case Study: The CUBL-CF Compact Flame Burner	Process Flare Regulations and Fundamentals	Case Study: The nViro XSR Elevated Steam Flare
11:00 AM CDT	Process Burner Installation, Repair and Maintenance		Process Flare Inspection, Repair and Maintenance	Case Study: The Galaxy Multi-Point Ground Flare
3:00 PM CDT	Process Burner and Heater Combustion Fundamentals	Case Study: The CUBL-CF Compact Flame Burner	Process Flare Regulations and Fundamentals	Case Study: The nViro XSR Elevated Steam Flare
4:00 PM CDT	Process Burner Installation, Repair and Maintenance	_	Process Flare Inspection, Repair and Maintenance	Case Study: The Galaxy Multi-Point Ground Flare

Callidus Technologies – Leader in combustion solutions



Honeywell Internal

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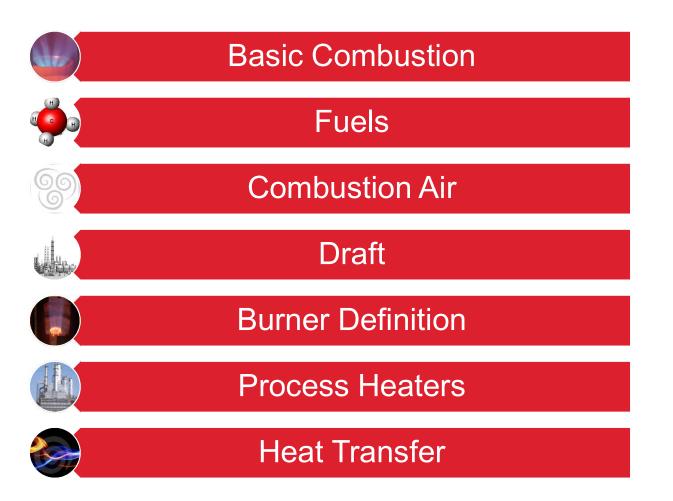


BASIC COMBUSTION & GENERAL HEATER OPERATIONS

STEFANO BIETTO SENIOR BUSINESS LEADER

2020 CALLIDUS BURNER SCHOOL | VIRTUAL, ONLINE, EVERYWHERE

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WHAT IS COMBUSTION?

A chemical reaction between fuel and oxygen producing heat.

CO2

Carbon Dioxide

Air is usually the source of oxygen.

202

Oxygen

The chemical reaction produces "flue products."





CH₄

Methane

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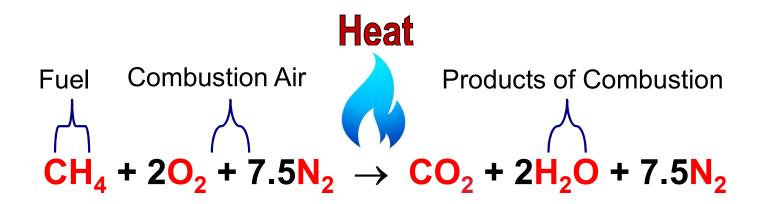
+ Heat

2 H₂O

Water

+

EXAMPLE: COMBUSTION OF METHANE





FUELS - TYPICAL GASEOUS FUEL COMPONENTS

- Methane CH₄
- Ethane C_2H_6
- Ethylene C_2H_4
- Propane C_3H_8
- Propylene C_3H_6

Butane – C_4H_{10}

Pentane – C_5H_{12}

 $Hydrogen-H_2$

Carbon Monoxide – CO

Hydrogen Sulfide – H_2S

Ammonia – NH₃

Carbon Dioxide – CO₂

Nitrogen – N₂

Water Vapor – H₂O



FUELS - BRITISH THERMAL UNIT



The British Thermal Unit is the amount of heat required to raise the temperature of one pound of water 1°F.

1 Btu/hr = 0.29 W 1,000,000 Btu/hr = 0.29 MW



FUELS - HEATING VALUES

Higher (Gross) Heating Value (HHV)

 The total heat available from combustion of a fuel with a source of oxygen, both 60°F when combustion starts, after combustion is complete

Lower (Net) Heating Value (LHV)

 The higher heating value minus the latent heat of vaporization of the water vapor formed by the combustion of hydrogen in the fuel

Burners in Process Heaters applications are usually specified in LHV

FUELS - HEATING VALUES

Heating Value in Btu/ft ³	LHV	HHV
Methane (CH ₄)	911	1012
Ethane (C ₂ H ₆)	1622	1773
Propane (C ₃ H ₈)	2322	2524
Butane (C ₄ H ₁₀)	3018	3271
Hydrogen (H ₂)	275	325
Carbon Monoxide (CO)	321	321



COMBUSTION AIR

Dry air is primarily a mixture of oxygen and nitrogen with approximately 21% oxygen and 79% nitrogen

The other major component of air is water vapor. For high ambient temperature the water vapor content of moist air can approach 5%. Significant water vapor in combustion air will affect burner performance.



TYPES OF FUEL/AIR MIXTURES









TYPES OF FUEL / AIR MIXTURES

Stoichiometric Mixture

•What can occur if you operate with the exact amount of air?

- -If fuel conditions change may run burner out of air
- -The mixing residence time in a furnace is limited, may not get good mixing before leaving the radiant section

Lean Mixture (excess air)

•What can occur if you operate with too much excess air?

-The furnace will operate inefficient (will take more heat input to heat up the excess volume of air

Rich Mixture (excess fuel)

•What can occur if you operate with too little excess air?

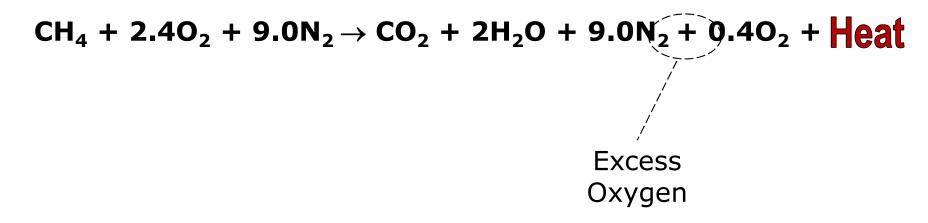
-Will generate CO

-Could be unsafe operating conditions



LEAN MIXTURE (EXCESS AIR)

When air is supplied in an amount that is in excess of the amount required to complete the combustion reaction with the fuel, the additional air is called excess air. The following chemical equation illustrates the burning of methane with 20% excess air.





PROCESS BURNER (AIR REQUIREMENTS)

For a specified burner heat release, the quantity of air required is essentially the same for all hydrocarbon fuels and fuel mixtures. When a significant quantity of hydrogen is present, the required air will be less.

Rule of thumbs (hydrocarbon fuels):

- 1 MMBtu/hr requires 10,000 ft³ of air.
- The excess air is approximately five times the measured oxygen in the dry combustion products if no inert components are present in the fuel.



DRAFT – HEATER STACK Two major purposes served by the stack:

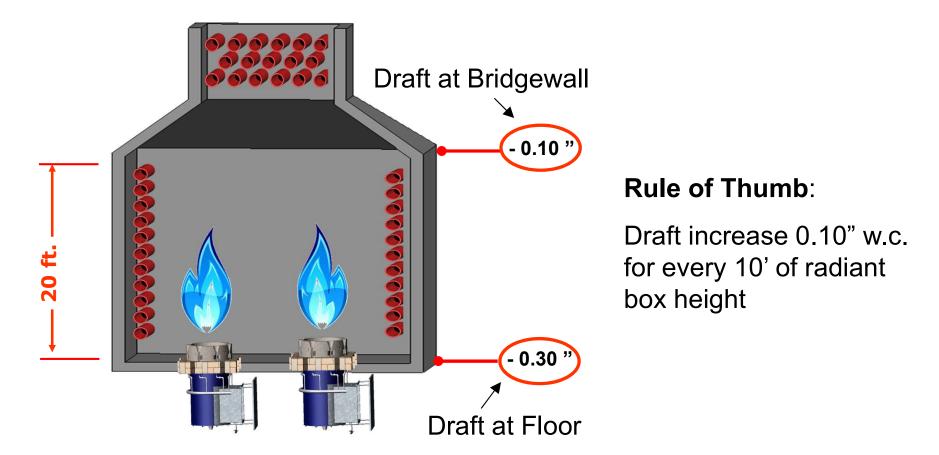
- 1. Provide a point of discharge for combustion products
- 2. Provide a negative pressure inside the furnace



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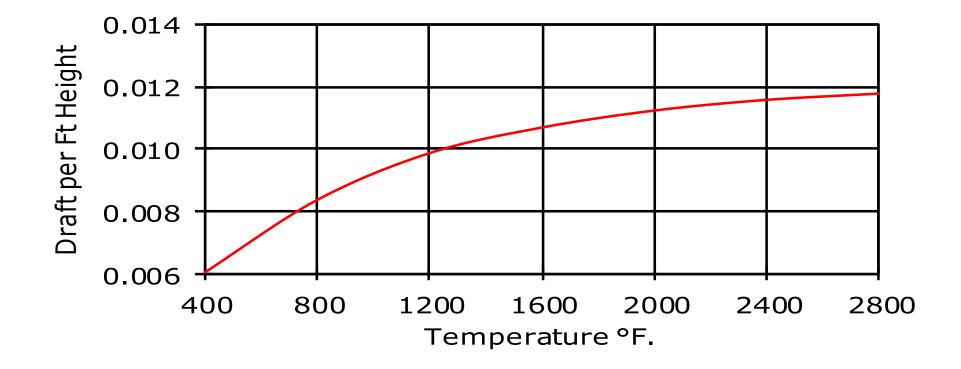
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DRAFT - PROCESS HEATER





PROCESS HEATER (DRAFT)





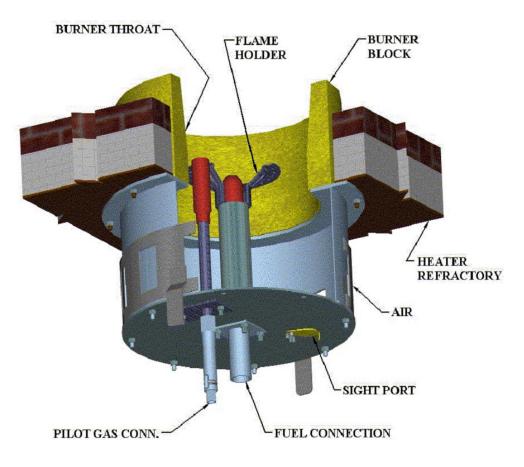
PROCESS BURNER (DEFINITION)

A burner is a device that delivers fuel and air in proper proportions and with sufficient mixing energy to a combustion zone where continuous ignition, complete combustion, and proper positioning of the flame is maintained.





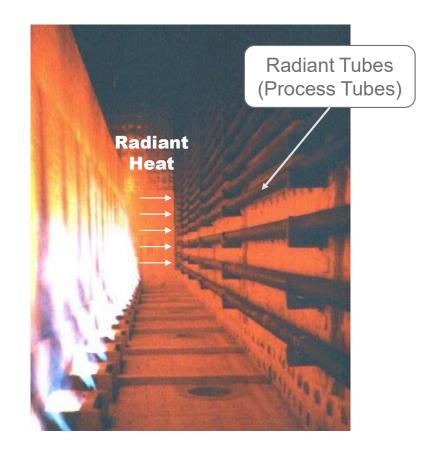
PROCESS BURNER (TYPICAL BURNER)





PROCESS HEATER

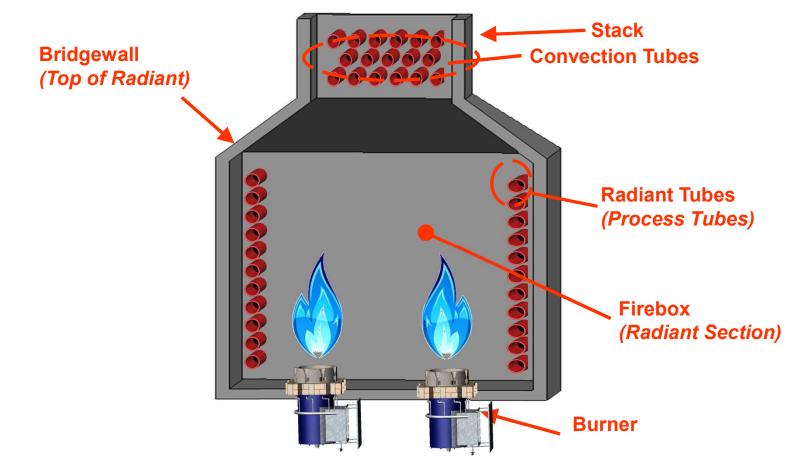
The purpose of a process heater is to heat the process side material by transferring heat from the hot combustion products to the process side material



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PROCESS HEATER (TERMINOLOGY)





PROCESS HEATER (HEAT TRANSFER)

The purpose of a process heater is to heat the process side material by transferring heat from the hot combustion products to the process side material.

Two Types of Heat Transfer:

- 1. Radiant Contact with the hot gases is not necessary for radiant heat transfer. Radiant heat transfer is a function of the gas temperature and the ability of the hot gases to radiate energy.
- 2. Convective Contact with the hot gases is necessary for convective heat transfer. Convective heat transfer is a function of the temperature of the hot gases and the velocity of the hot gases across the tube surfaces.



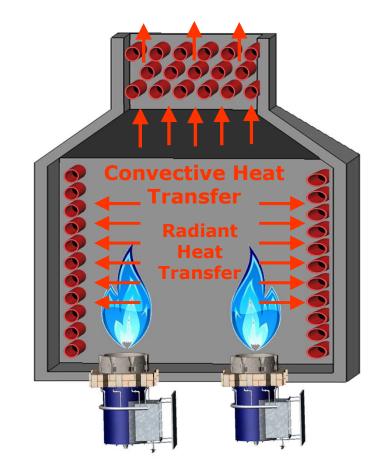
PROCESS HEATER (HEAT TRANSFER)

Convective heat

transfer occurs to the convection tubes because of the combustion product temperature and velocity

Radiant heat

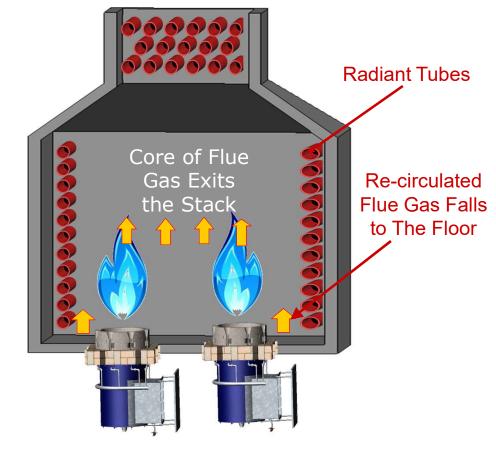
transfer occurs to the radiant tubes because of the ability of the hot gases to radiate energy. Some convective transfer also occurs to the radiant tubes



PROCESS HEATER (FURNACE FLOW PATTERNS)

•A core of hot Flue Gases exit the furnace stack

• The Flue Gases along the process tube boundary are cool and dense & re-circulate to the furnace floor





TYPICAL HEATER APPLICATIONS (PROCESS BURNERS)

Refinery



- Refining crude oil into useful products
 - Liquefied petroleum gas (LPG)
 - Gasoline or petrol
 - Kerosene
 - Jet fuel
 - Diesel oil
 - Fuel oil

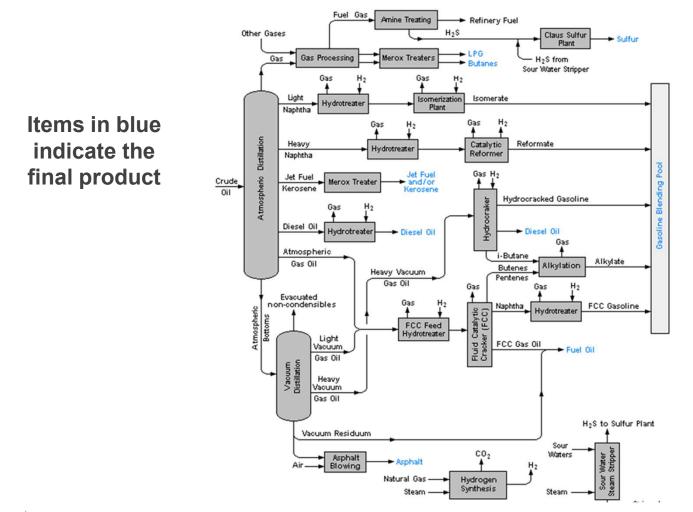
Petrochemical Plant



- Converting N.G. or petroleum liquids into useful intermediate and final products
 - Fertilizers
 - Olefins
 - Adhesives
 - Detergents and Solvents
 - Rubber and Elastomers
 - Films and Fibers
 - Polymers and Resins



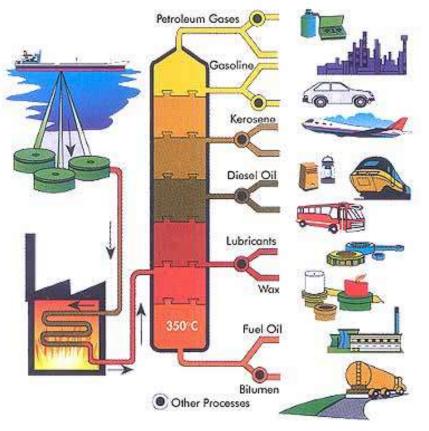
TYPICAL REFINERY PRODUCTION



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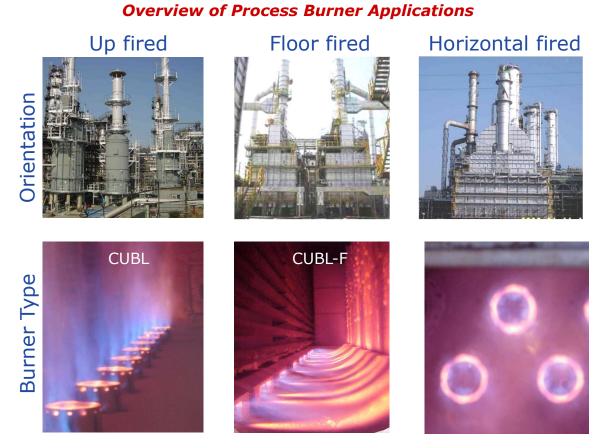
TYPICAL REFINING PRODUCTS

So what products are generated from Process Heaters?





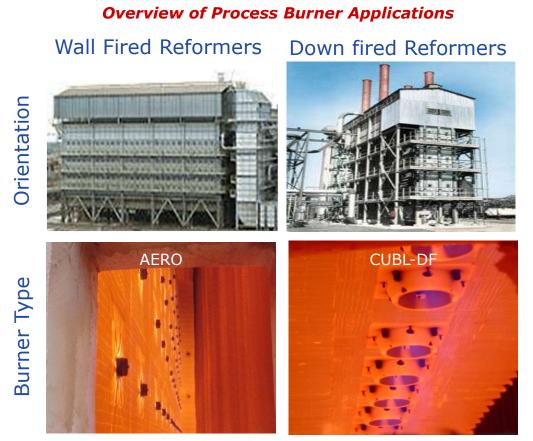
REFINERY HEATERS (FIRING ORIENTATIONS)



Typical Furnace Operating Temperature 1300 to 1650 Deg. F.



PETROCHEMICAL APPLICATIONS (REFORMERS)

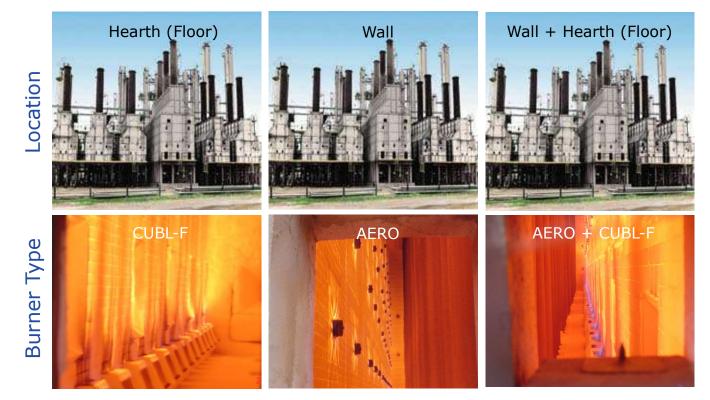


Typical Furnace Operating Temperature 1800 to 1900 Deg. F.



PETROCHEMICAL APPLICATIONS (CRACKING FURNACE)

Overview of Process Burner Applications



Typical Furnace Operating Temperature 2200 to 2300 Deg. F.

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BURNERS	PARTS	FLARES	
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Jesse Chambers	Brian Yeates	Kurt Kraus	
	Albert Septiano		





PROCESS BURNER TROUBLE SHOOTING

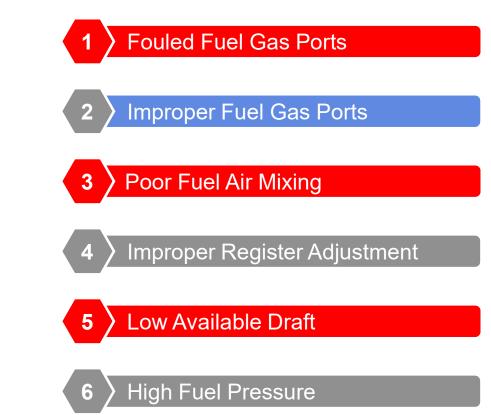
JESSE CHAMBERS

SENIOR TECHNICAL SALES ENGINEER

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AREAS OF CONCERN





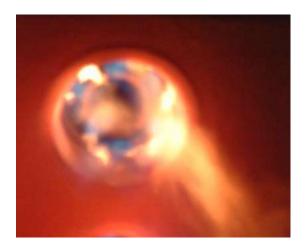
PROBLEM: IRREGULAR FLAME PATTERNS Indications

- One side of flame pattern is long, the other side is short
- Flames lean toward the tubes

Effects

- High tube skin temperature
- Increased rate of tube coking or failure
- Hot tube hangers
- Decreased heater capacity
- High CO levels
- Increased fuel usage
- High excess air

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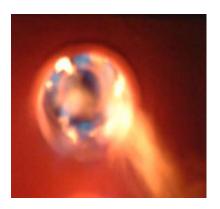


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PROBLEM: IRREGULAR FLAME PATTERNS

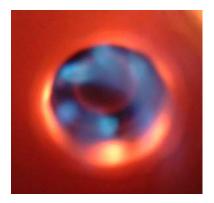
Cause

- Poor fuel
- Air distribution and fuel
- Air mixing



Solution

- Clean gas tips
- Adjust all burner air registers to same setting
- Check gas tip alignment





PROBLEM: HIGH GAS PRESSURE

 Fuel gas pressure is higher than design

Effects

 Failure to get proper outlet temperature on process side





PROBLEM: HIGH GAS PRESSURE Cause Solution

- Plugged fuel tip ports
- Partially closed burner block valves
- Change in fuel composition

- Clean fuel tip ports
- Open individual burner block valves
- Replace burner tips that are designed for new fuel gas composition



PROBLEM: BURNER FAILS TO LIGHT OFF Indications

Operator cannot ignite burner

Effects

• Failure to get unit started up



PROBLEM: BURNER FAILS TO LIGHT OFF

Cause

- Pilot flame does not "contact" flammable mixture
- No fuel flow to burner
- High air flow to burner
- Improper fuel/air mixing

Solution

- Reposition pilots to locate as specified on drawings
- Ensure all block, safety shut-off and flow control valves are open and in proper position
- Close air register to recommended ignition position (Standard practice)
- Check orientation of fuel tips and clean fuel tips



PROBLEM: PULSATING FLAME Indications

- A "woofing" noise
- Erratic flames
- Back firing through burner register

Effects

- Damages refractory, tubes, tube supports, and other components
- Destroys burner
- Loss of flame
- Possible explosion



PROBLEM: PULSATING FLAME

Cause

- Insufficient combustion air
- Poor fuel/air mixing

Solution

- Reduce fuel flow until heater has sufficient air to burn gas within heater
- Check draft to ensure not too high
 - If yes, reduce draft so the burner damper can be opened to allow the pressure drop to be taken across the throat rather than the air register



PROBLEM: OVERHEATING IN CONVECTION SECTION Indications

- Refractory falls from roof
- Structural steel is warping and opening up

Effects

- Reduced capacity
- Unit is shut down because of overheating



PROBLEM: OVERHEATING IN CONVECTION SECTION

Cause

- Positive pressure below the convection section
- After burning in convection

Solution

- Open stack damper to increase draft from positive to slightly negative pressure of 0.05" H₂O
- Check excess O2 at top of radiant section
- Check for leaks in furnace

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